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R E M A R K S

Referring to ¶4 "'exothermic reactor'" has been changed to "'reaction'", so antecedent is found at line 7 of claim 1. Claims 6, 7 and 9 have been amended, as helpfully suggested, to avoid '112 objection. Claims 13 and 14 have been cancelled.

Reconsideration and withdrawal of the rejection of remaining claims is respectfully urged in view of the following:

A. Inventor's further comments, attached, stress technical design philosophy differences, and motivation, as between endothermic and exothermic reaction conditions, as affecting practical apparatus and its operation.

B. The combination of claim 1 which includes the steam generator, surrounded by a helical catalyst bed, external to the generator, is not suggested by Collins, or Amano. (Collins lacks a helical catalyst bed, his generator is not centrally located to be entirely outside his bed, and Amano lacks a steam generator.) Motivation to combine Collins and Amano is lacking because Amano does not teach removal of exothermic heat

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to an inner centrally located steam generator; and Amano is concerned with endothermic reforming reactors (see page 1 of inventor's comments).

C. Collins teaches LTS (low temperature shift) reaction using multiple LTS reactors disposed in a steam generator, so therefore he does not suggest an LTS reactor disposed outside of an inner steam generator.

D. Motivation to combine Collins and Amano is therefore lacking, due to fundamental differences between endothermic and exothermic hot flow systems.

E. The specific temperature ranges and gas velocities of claims 2, 7, 8 and 10 (claim 7 now based on claim 2) for this exothermic heat transfer system are nowhere suggested by Collins or Amano.

Allowance is urged. The interview on August 23 is acknowledged.

Respectfully submitted,



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WWH:ts
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